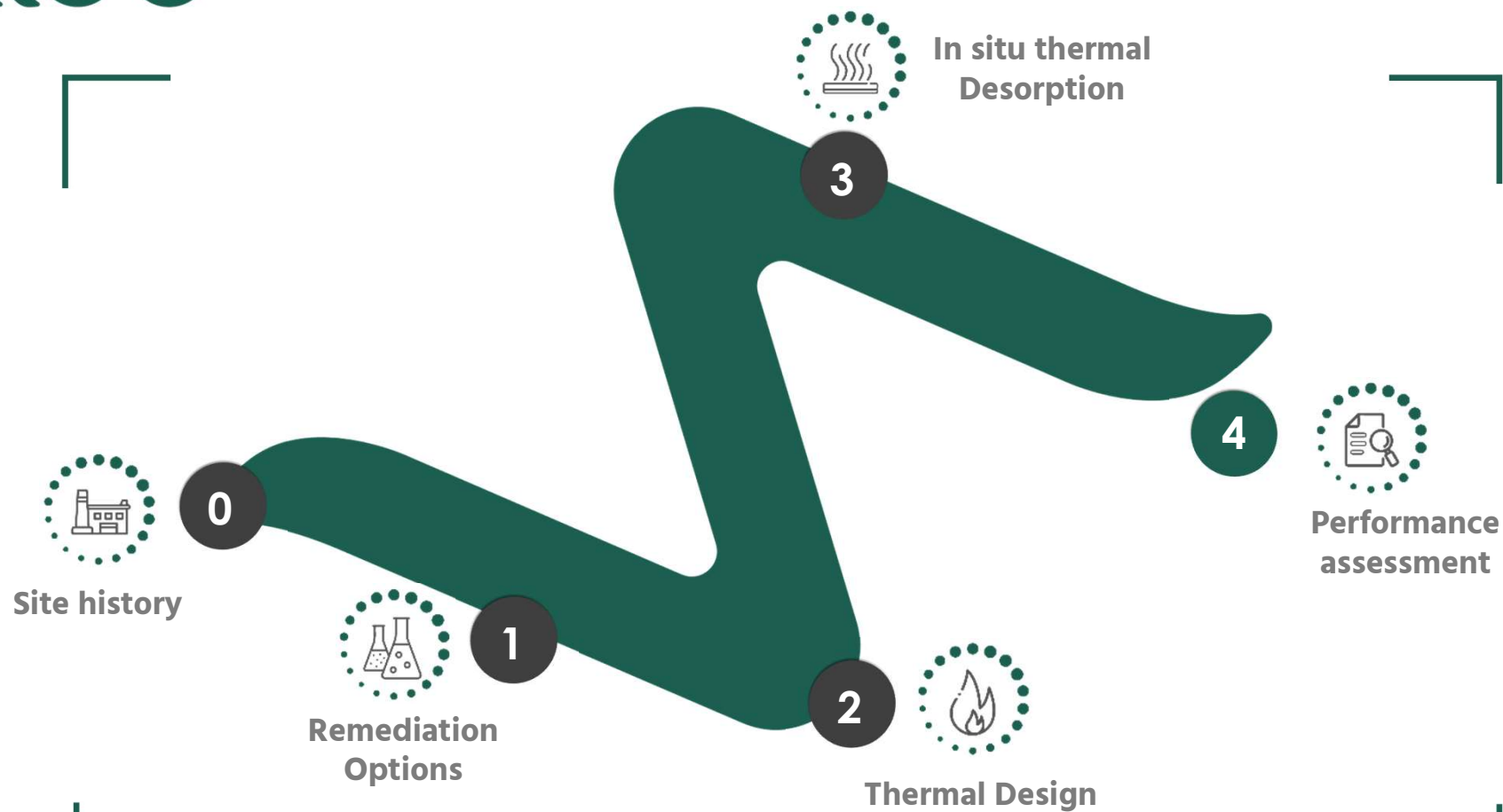
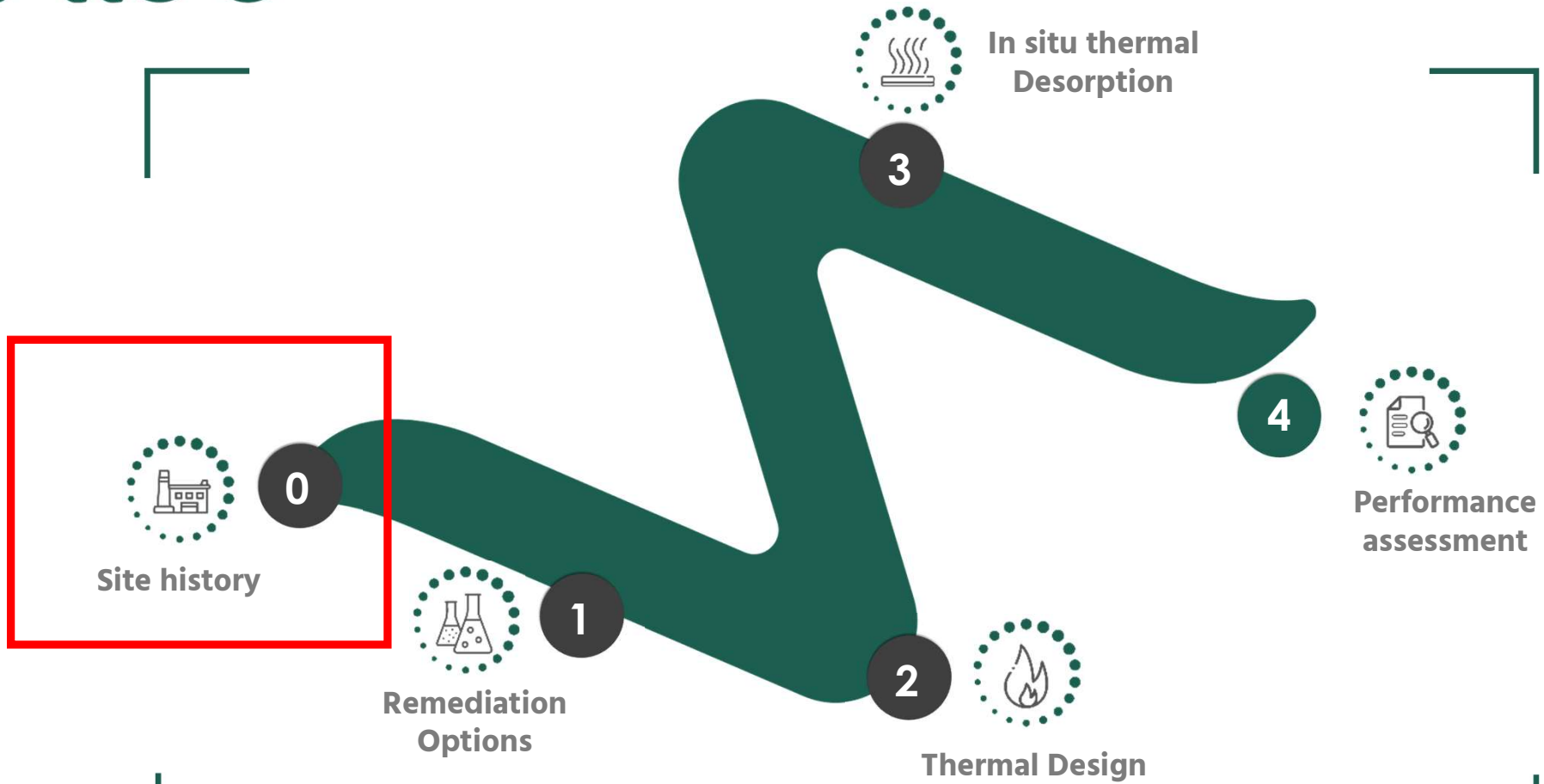




# Mercury in situ remediation by Thermal desorption

Matthieu Sangely / Pierre-Louis Guillerm





# Site History

- 1922 – Start of site activities on agricultural lands
- 1928 to 1961 – Chemical production using mercury as catalyst → 2 former ovens for regeneration of the catalyst plus probable discharge of mercury-containing waste in a series of sumps
- 1961 – New chemical process without mercury as catalyst
- 2020 – Stop of all the activities and start of the dismantling process
- 2022 - 2023 – Assessment of feasibility of remediation options



**1961**



**1986**

# Site conditions

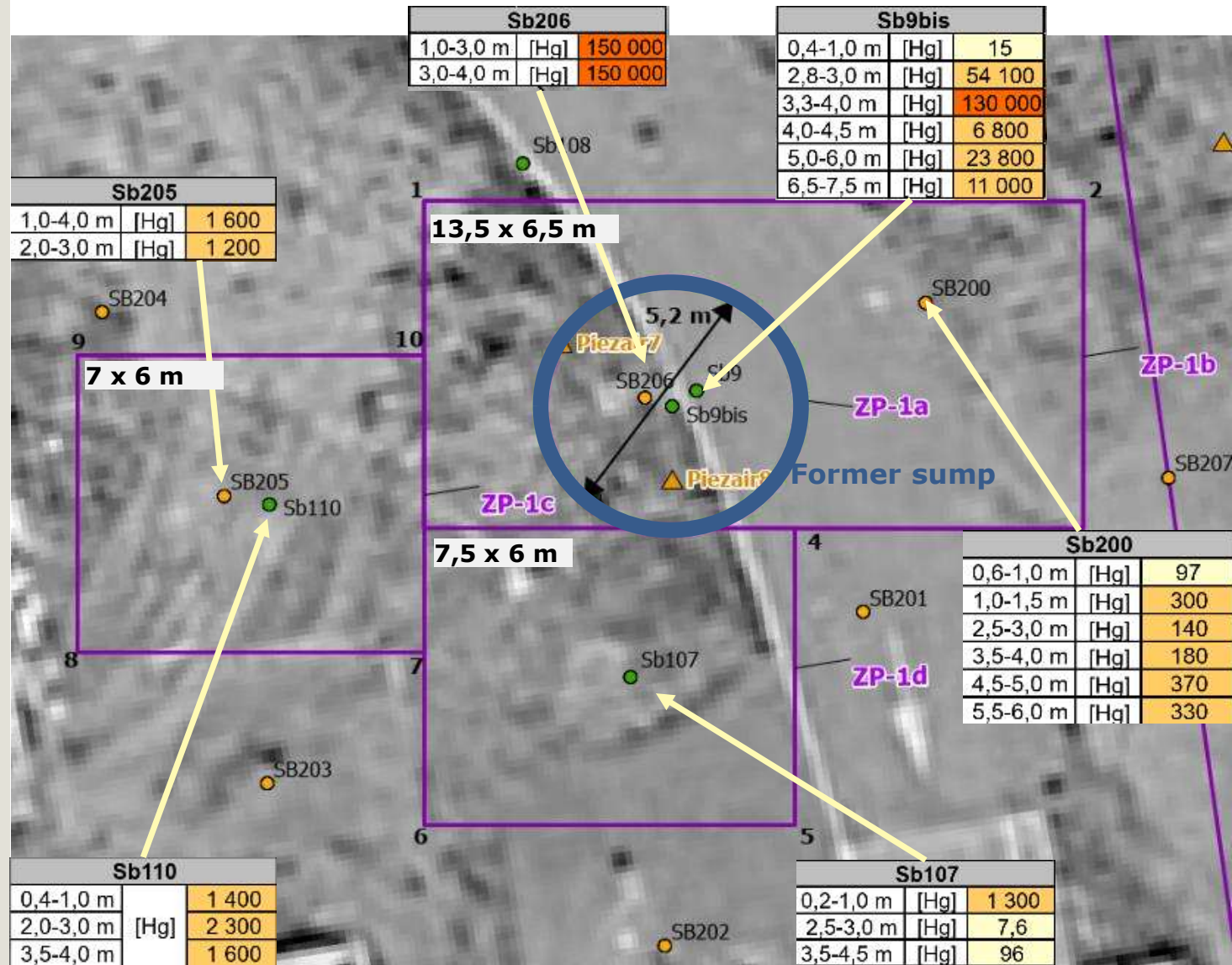
## Context : Site Closure

3 phases of investigations  
between 2020 and 2022

## Main findings at the sump area

- Elevated impact of mercury in soil (max = 150,000 mg/kg)
- Presence of mercury beads
- Impact depth (7m or more)
- Limited extension (150 m<sup>2</sup>)
- 2 tons of mercury estimated in this hotspot (95 % of total mass of mercury on site)
- Groundwater not impacted

RAMBOLL



Concentration in mg/kg



# Soil conditions

Sandy soil

75 to 90 % of dry matter

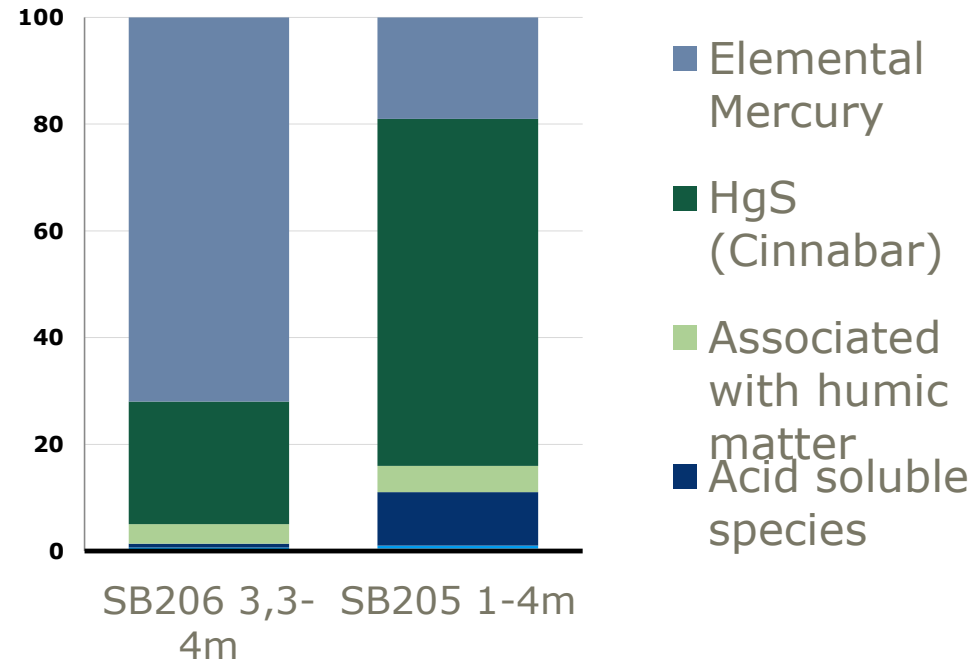
Mainly elemental mercury and Cinnabar (HgS)

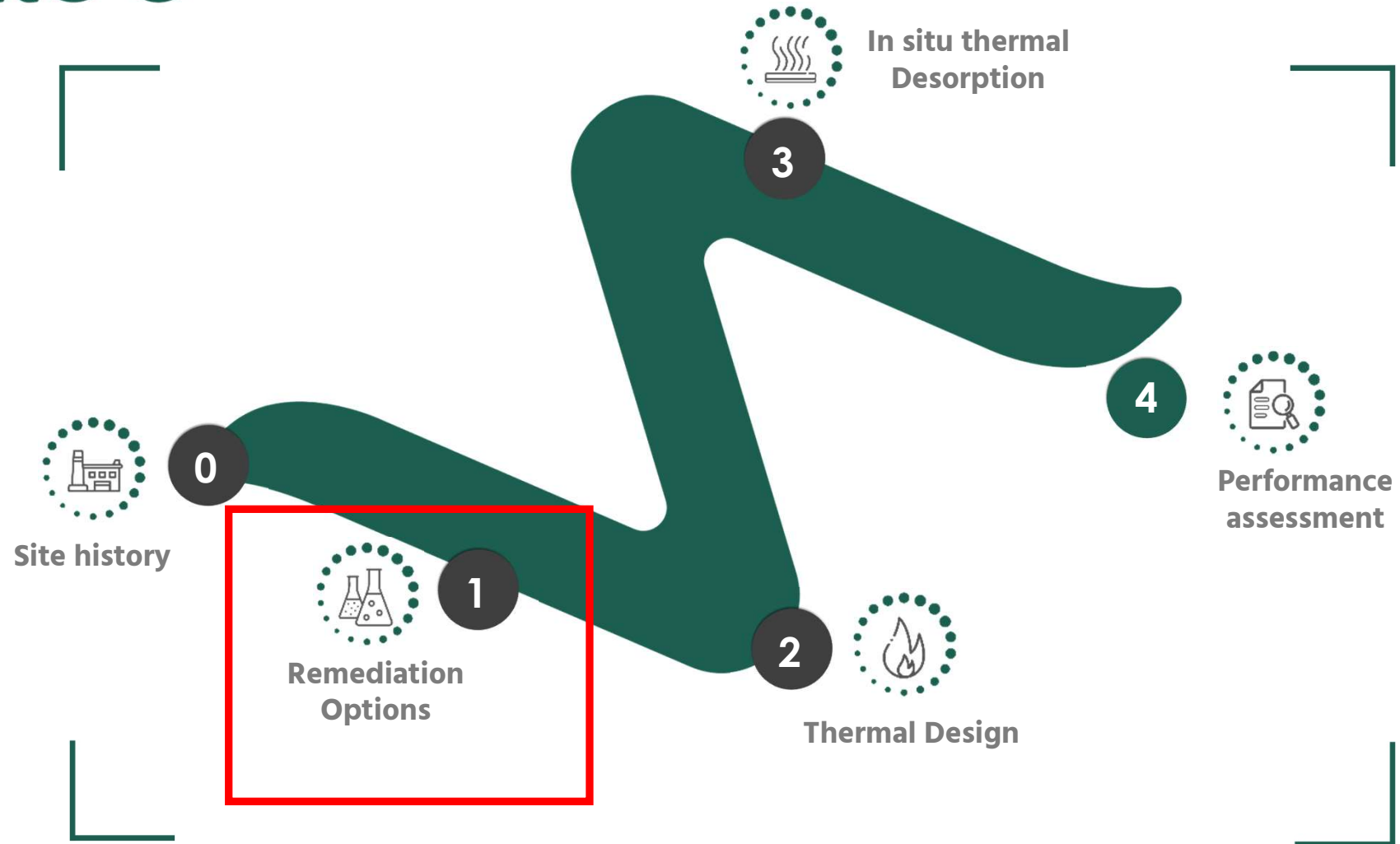
Rather insoluble mercury

Negligeable concentration of organic mercury



RATIO OF MERCURY SPECIES





# Remedial action plan

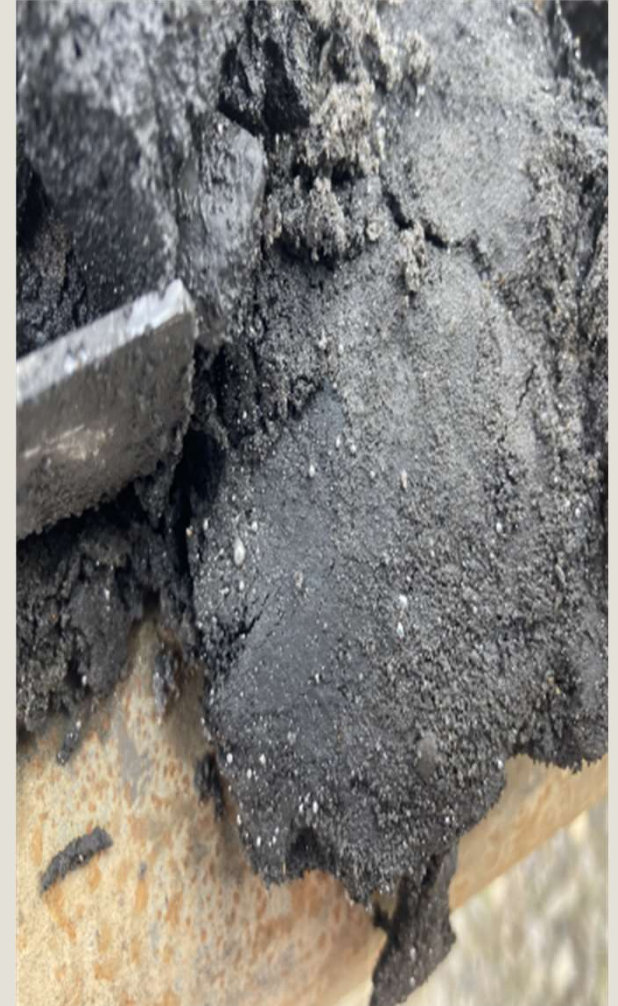
## French methodology requirement

→ Removal of the main hotspot

## 2 remedial options

- In-situ thermal desorption + venting + condensation of elemental mercury + off-site disposal (salt mine)
- Excavation at 10m depth (sheetpile) + on-site pre-treatment (stabilisation) + off-site disposal

**Feasibility studies in order to validate these 2 options**





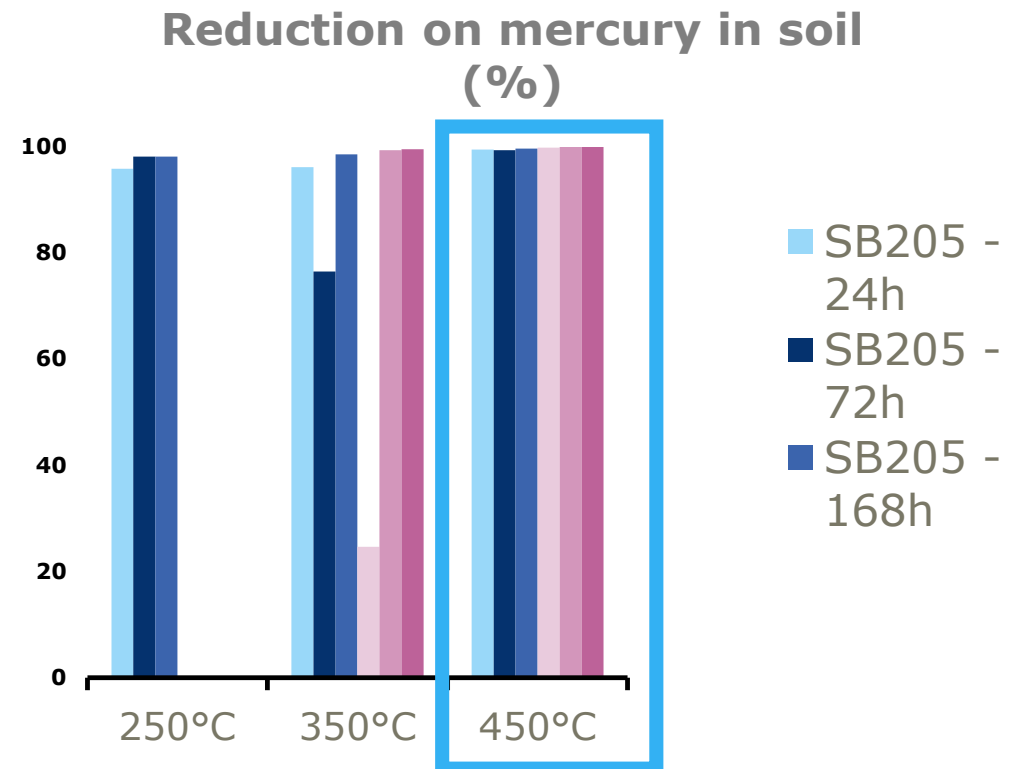
# Thermal treatment pilot test results (lab test)

Low soil thermal capacity: between 0.7 and 1.1 kJ/kg/°C  
→ less energy consumption than with standard soil

**Great efficiency at 450°C → up to 99.8% of reduction of mercury in soil with only 24h treatment**

Equivalent efficiency at 350°C with 7 days of treatment

**Nearly 100% of mercury were condensed** as elemental mercury, thus almost no additional costs for the treatment of gas emission or water



# Why was In-Situ Thermal Desorption chosen?

**Favorable site conditions** (homogenous sandy soil + restricted area)

**Great reduction of hazardous waste** in volume (2 t Vs 2,000 t)

Only **few contaminated soil movement** during the process → reduction of human exposition and risk of dispersion

Nearly **no need for backfilling material**



## How will the project contribute to the UN SDGs



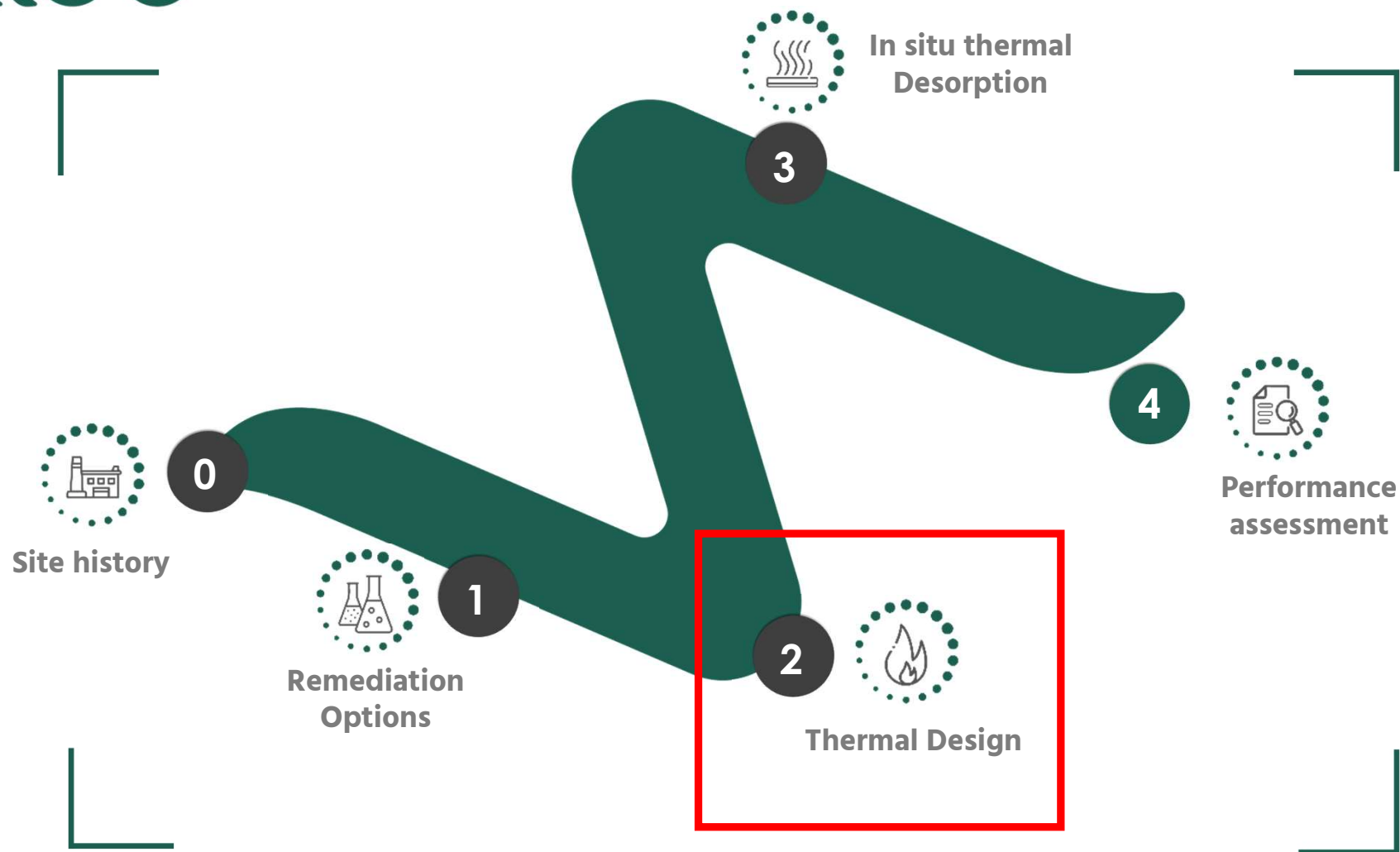
Responsible consumption and production

- low quantity of waste
- low need for backfilling materials and reduced transportation



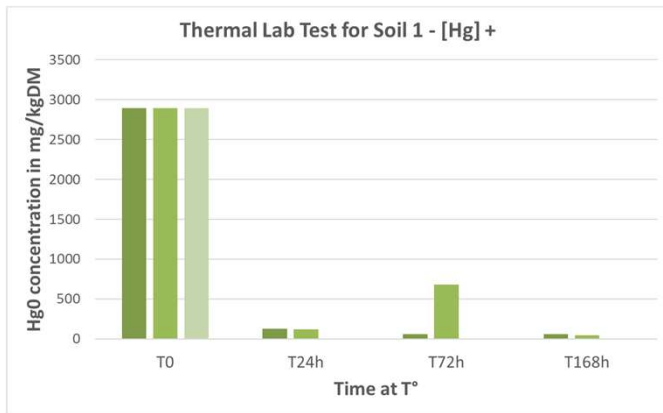
Good Health and Well-being

- Reduced potential exposure to volatile mercury during the treatment process



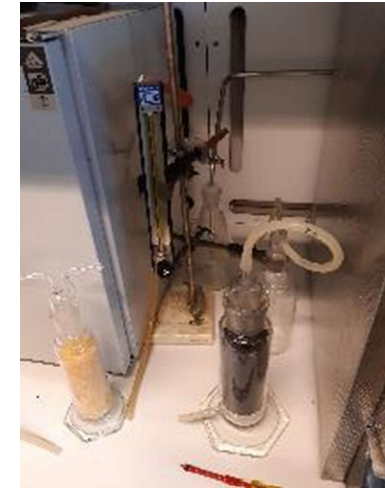
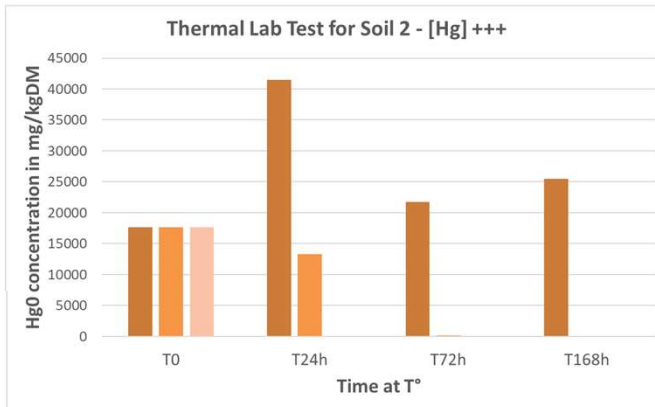
# Thermal design : 1st step → Lab Test

Several couples Temperature / Time are tested (Reminder Hg boiling point (BP) = 356,62 °C)



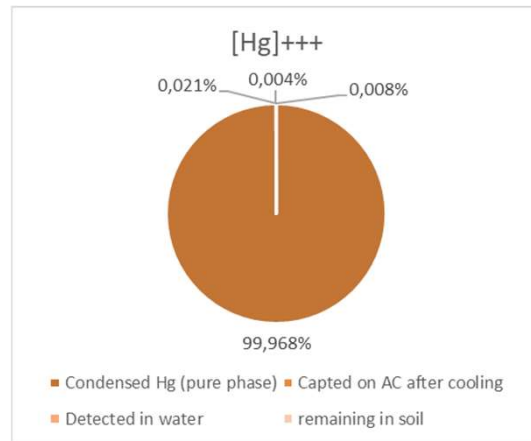
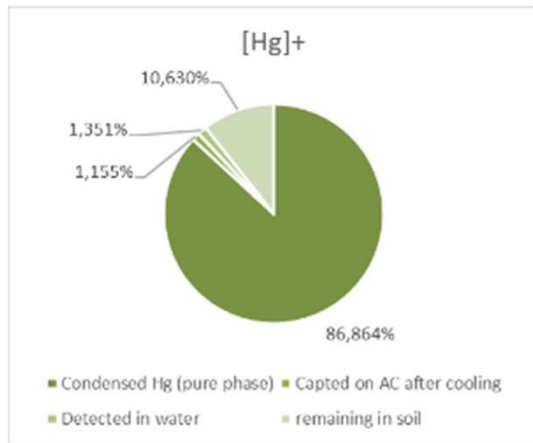
Medium concentrations:  
good results even at  $T^{\circ} < BP$ .  
At 450°C [Hg] < 15  
mg/kgDM after a week.

High concentrations:  
Best results at 450 °C  
([Hg] < 36 mg/kgDM) but  
still good results at 350 °C.

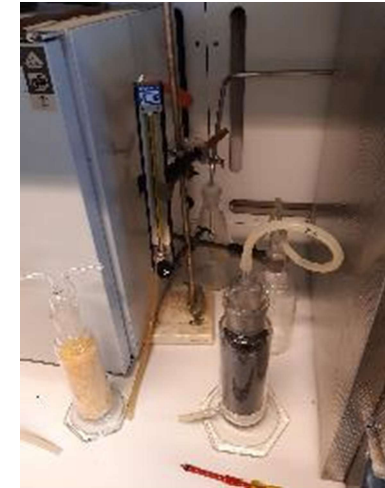


# Thermal design : 1st step → Lab Test

Partitioning of Mercury recovery



Nearly 100% of Mercury is condensed. Some heterogeneity due to Mercury form;  
Low AC consumption for fullscale





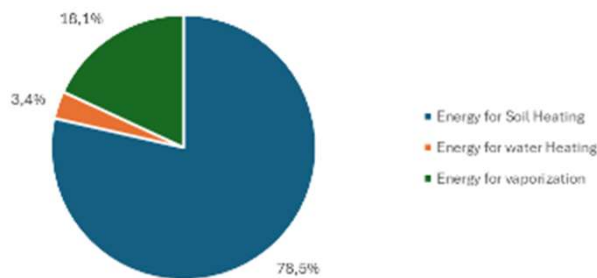
# Thermal design : Heating system

- Primary energy = Propane
- T°C aimed = 450°C
- Mass of soil to Treat = 2 421 T
- Mass of water in soil = 242 T

## Calculation for:

- 1- elevation of T° to 450 °C of soil;
- 2- elevation of T° to 100°C of H2O;
- 3- evaporation of H2O;

Usable Energy needed



## Efficiency led Strategy:

- Minimizing energy loss by insulation, by air flow AND by combustion air;

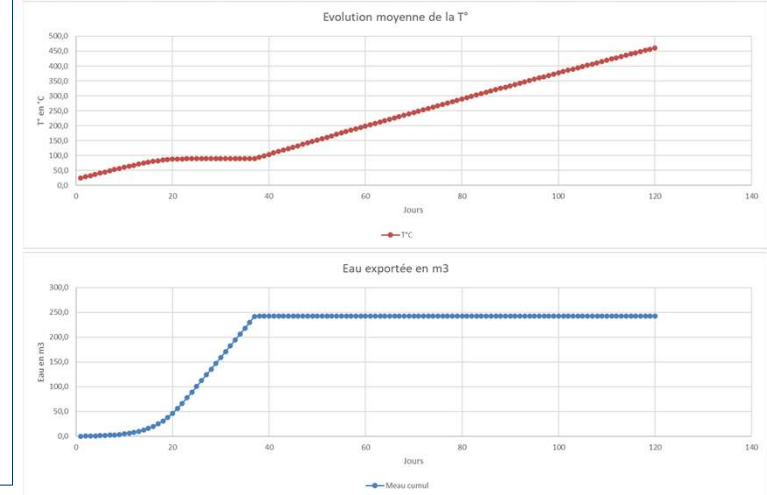
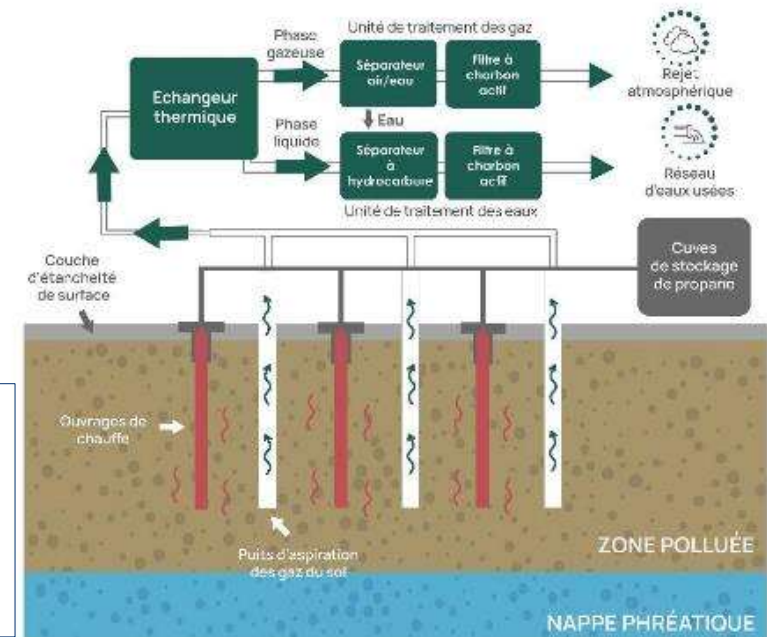
## Comparison between 2 strategies For 500 mW.h:

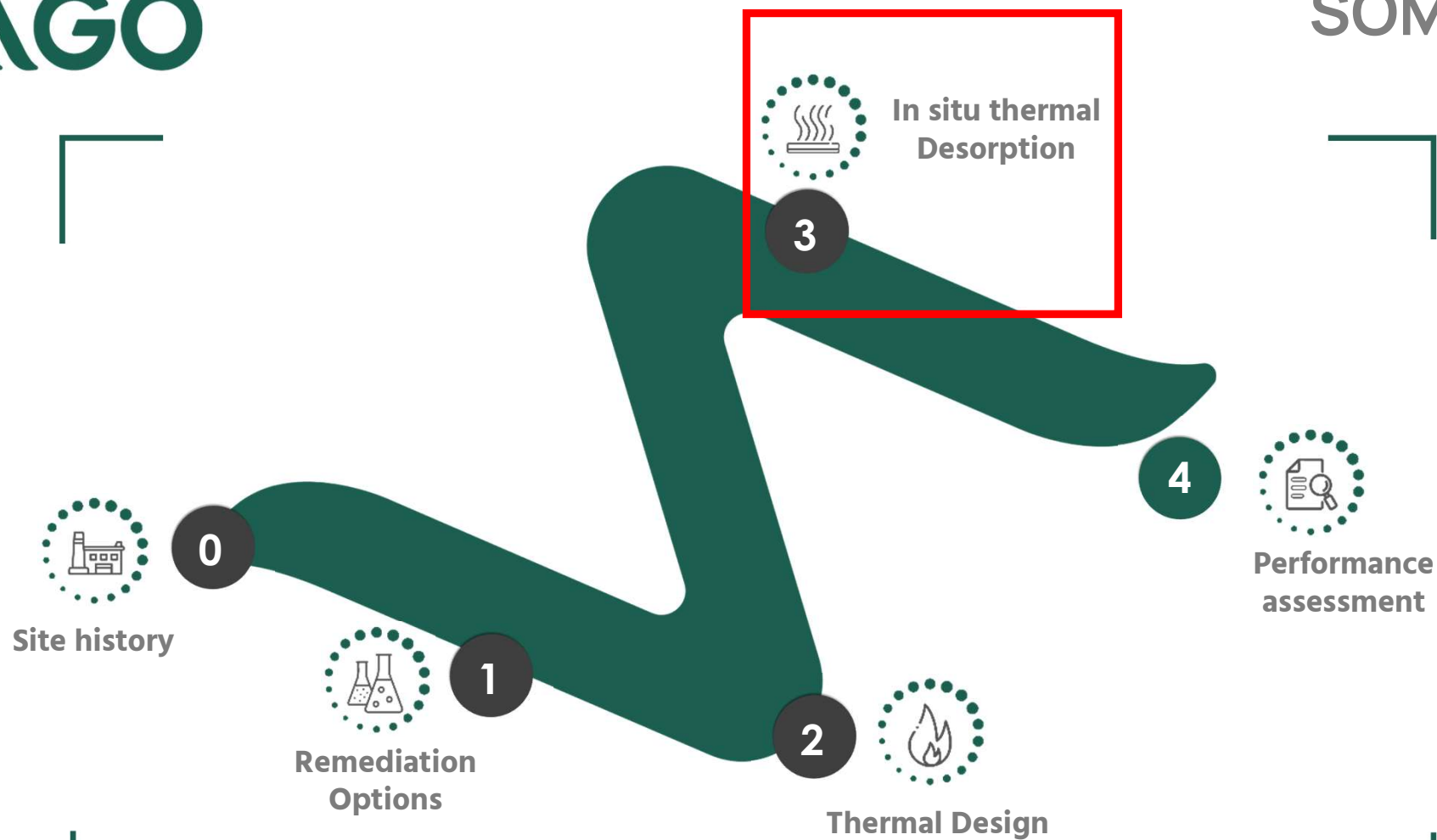
### Case 1

- 45 days → 463 kW;
- 23 burners ~20 kW;
- Mean T°C at Exhaust air ~500°C
- Energy loss = **40 %**

### Case 2

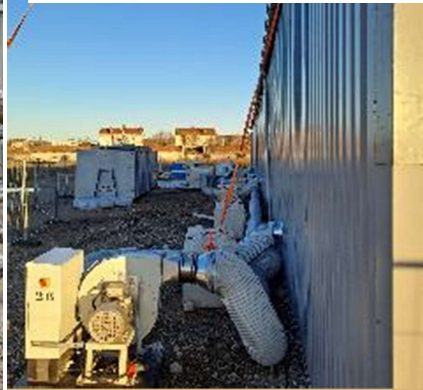
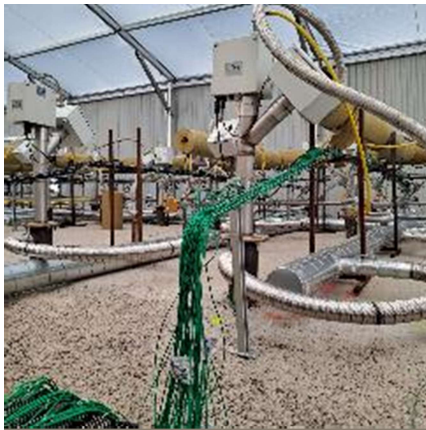
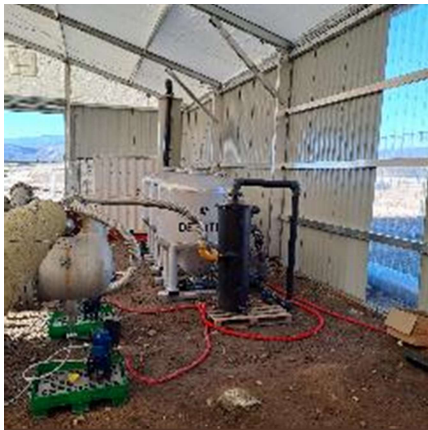
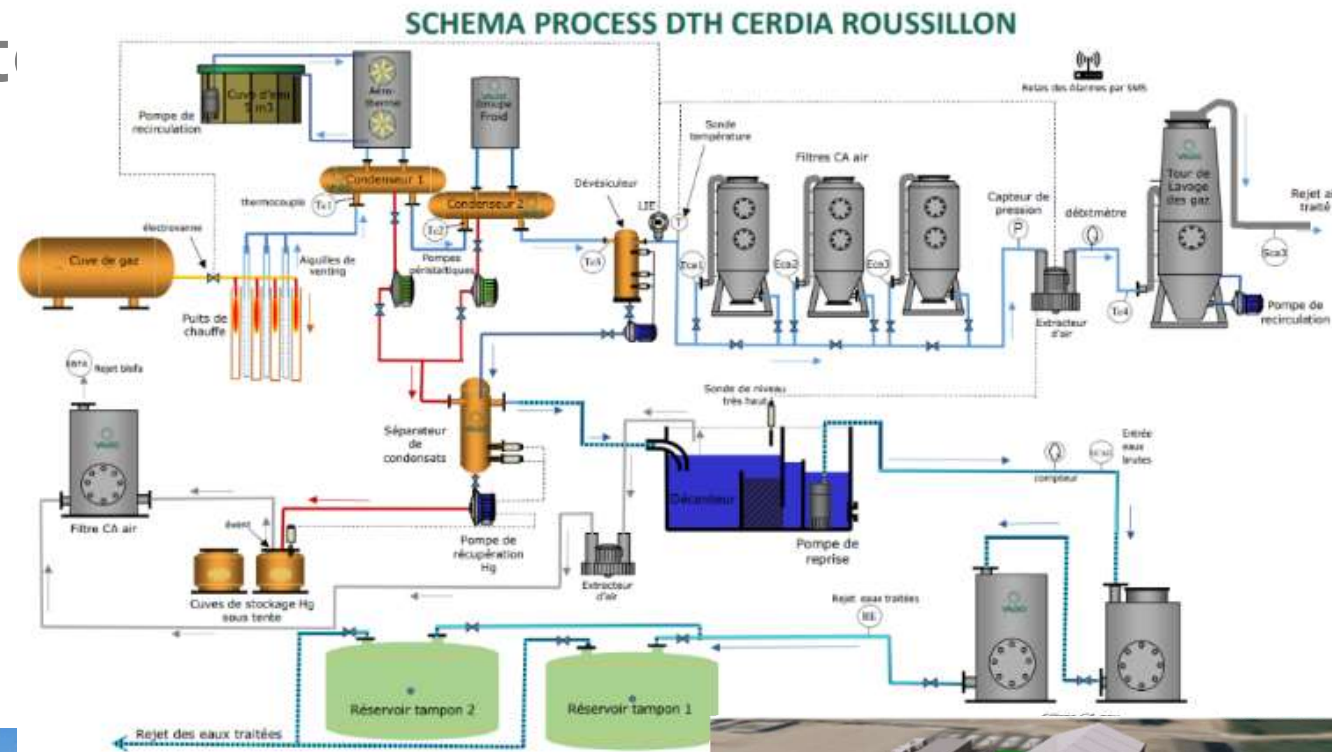
- 120 days → 174 kW;
- 9 burners ~20 kW;
- Mean T°C at Exhaust air ~300°C
- Energy loss = **24 %**



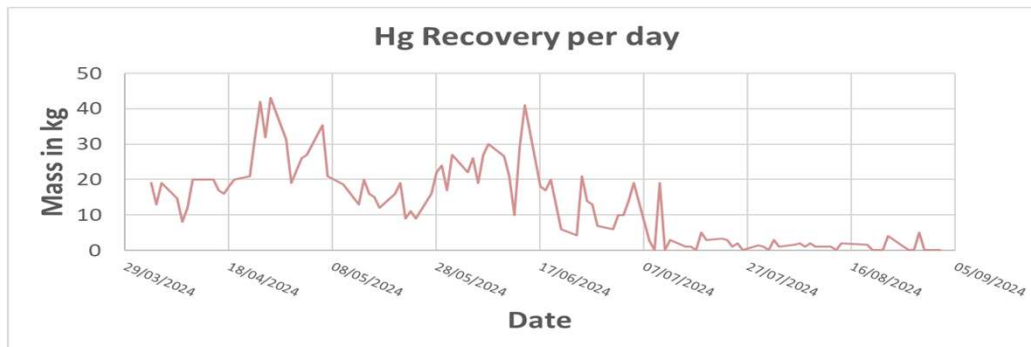
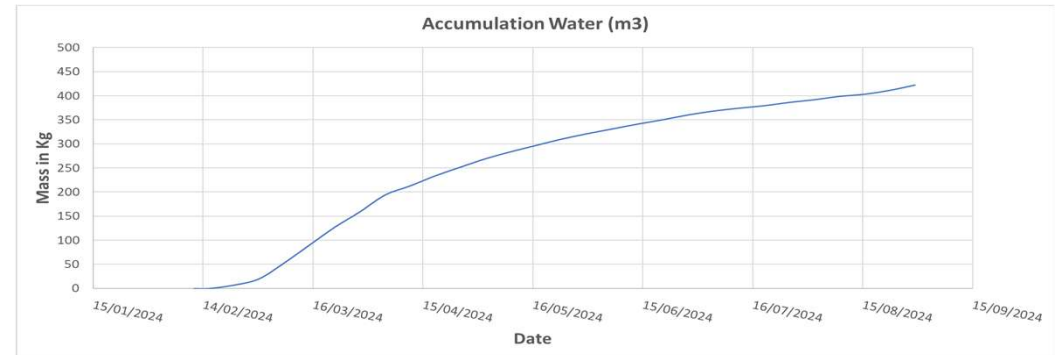
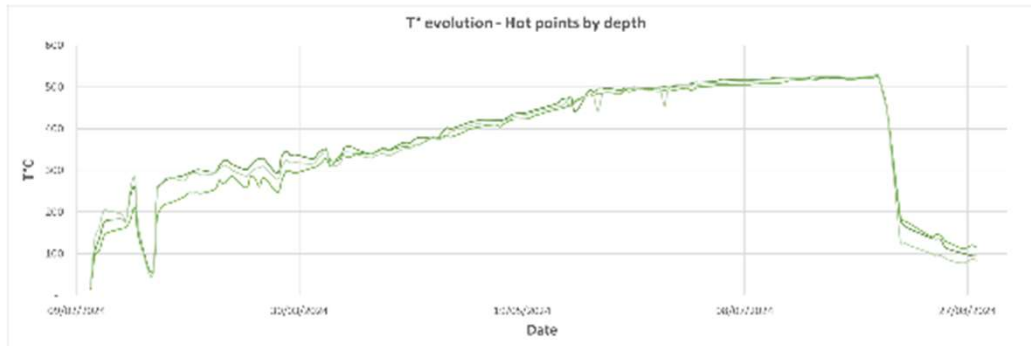


# Thermal Desorption syst

- 40 burners;
- 15 SVE wells;
- SVE systems ~700 m<sup>3</sup>/h
- 2 tubular exchangers
- 1 Chiller + 1 aerotherms
- 3 AC filters
- 1 washing tower



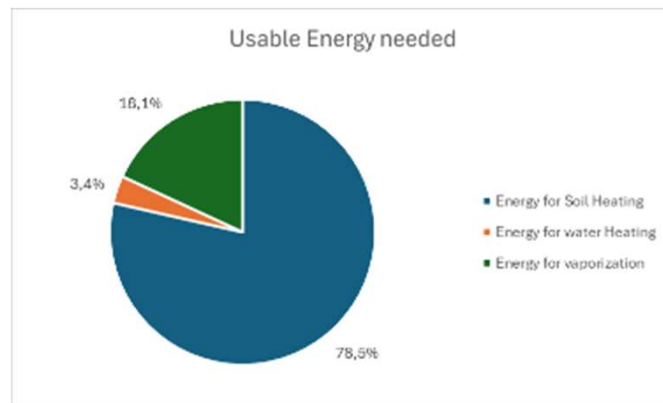
# Thermal Desorption Exploitation



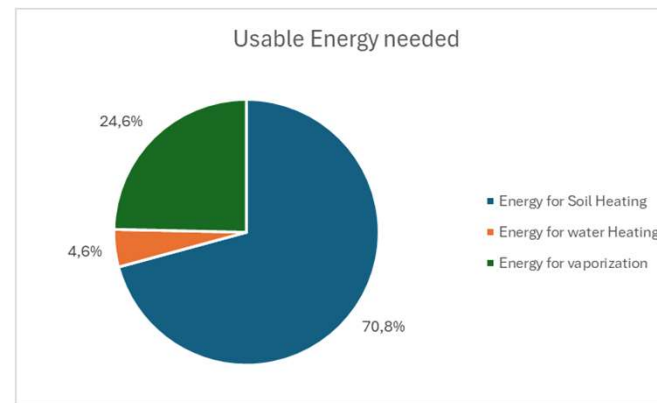
- Water is extracted after 10 days;
- Hg is recovered after 50 days;
- Slow increase of T°C on hot spots → energy savings;
- Nearly 2T of Hg is collected;
- 185 T of Propane consumed
- Max mean T° = 491 °C and 450 °C in cold points



# Thermal Desorption Comparison to model

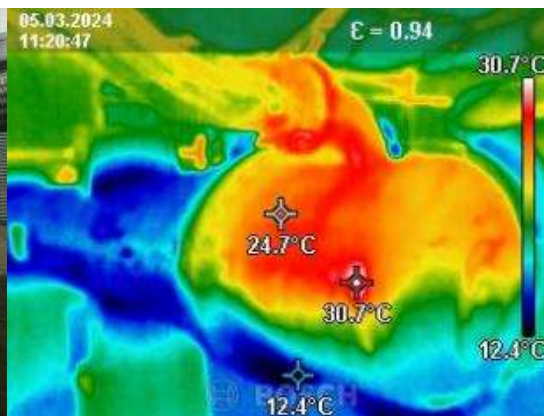


Projeté

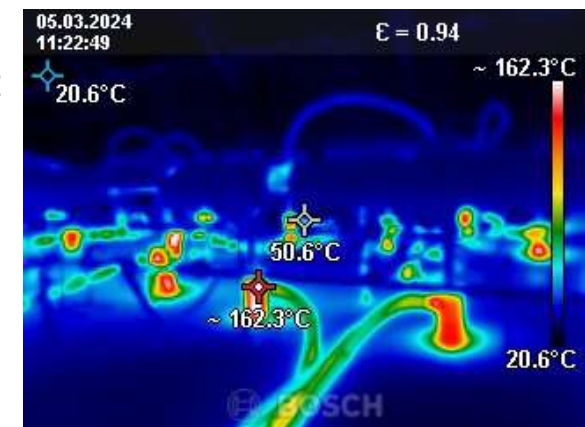


Realized

- Much more water than expected (+ 62 %)
- Hg is recovered after 50 days;
- Slow increase of T°C on hot spots → energy savings;
- Nearly 2T of Hg is collected in 140 days;
- 185 T of Propane consumed
- Max mean T° = 491 °C and 450 °C in cold points

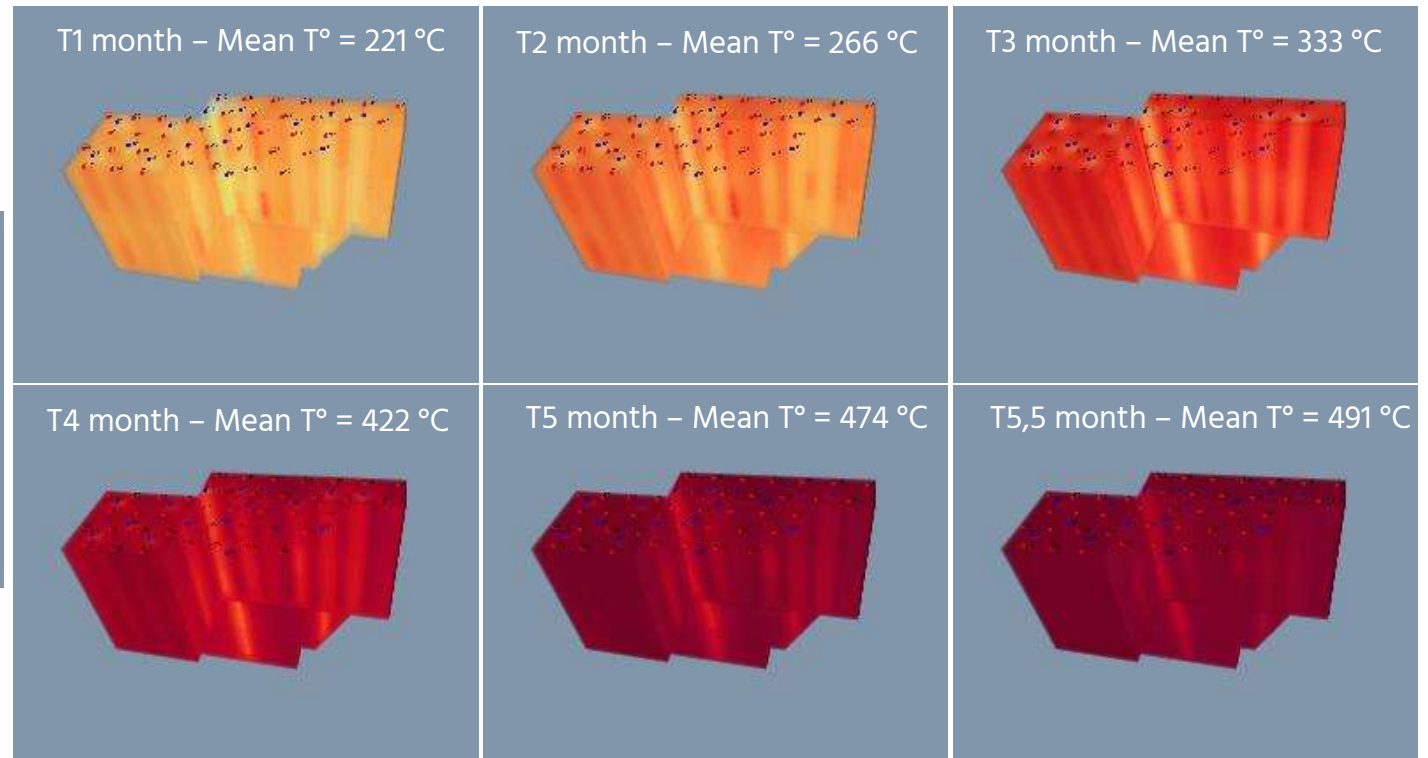
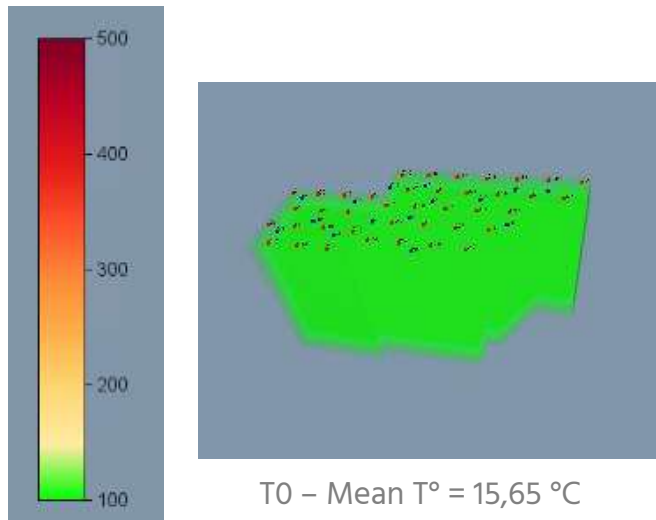


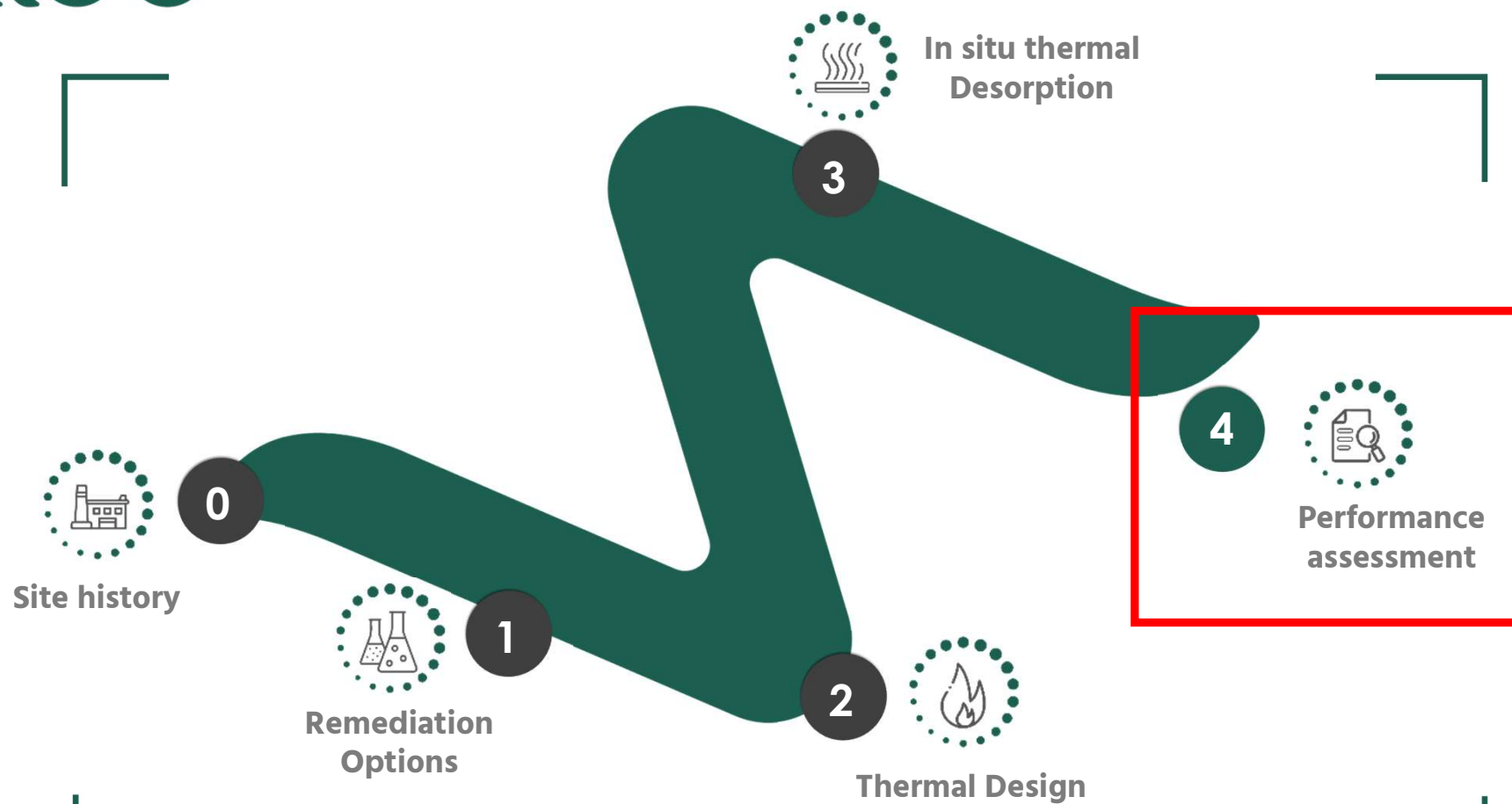
- SVE air treated at 12 °C  
→ Optimizing Ac performances;
- Control of insulation





# Thermal Desorption Comparison to model





# Objectives and monitoring of the ISTD

## Objectives

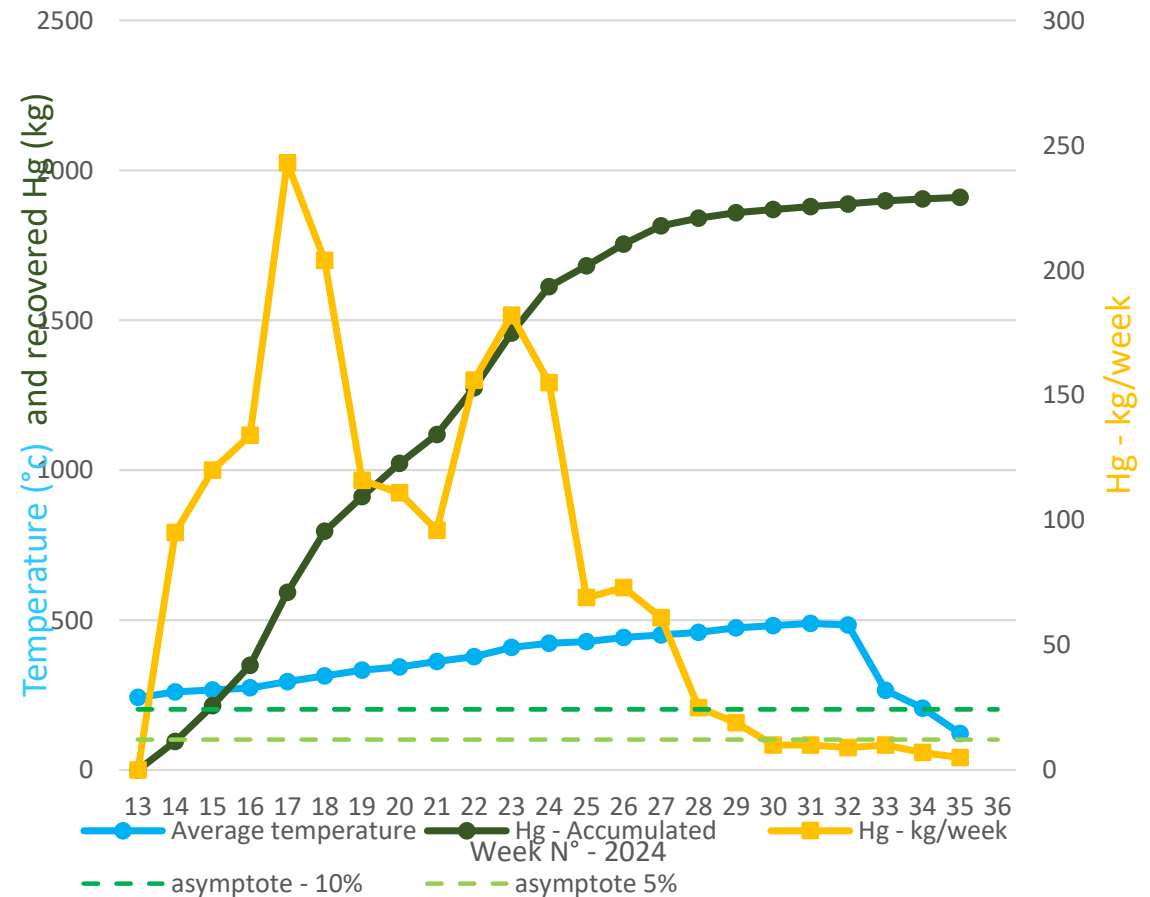
Reaching and maintaining 450°C on 95% of the sensors at the cold points, up to an asymptote for Hg recovery

### Asymptote

- Reached when recovered Hg <10% of Qmax Hg
- Treatment stopped when Hg recovered <5% of Qmax Hg over 14 consecutive days



## Temperature and recovered mercury monitoring



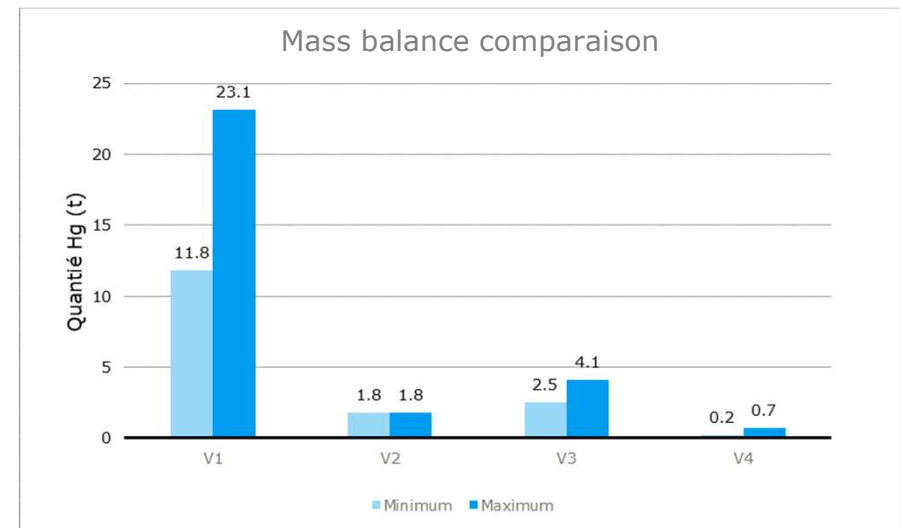
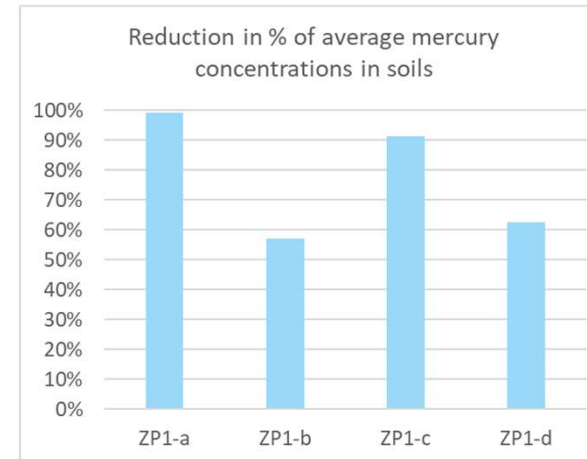
# Mass balance and Concentration reduction

|               | Mercury concentration in the soil before treatment |       |       |       |
|---------------|--|-------|-------|-------|
| [Hg] en mg/kg | ZP1-a  | ZP1-b | ZP1-c | ZP1-d |
| [Hg]min       | 15   | 2     | 221   | 4     |
| [Hg]moy       | 63 540   | 559   | 1 105 | 461   |
| [Hg]max       | 150 000  | 6 377 | 3 770 | 1 841 |

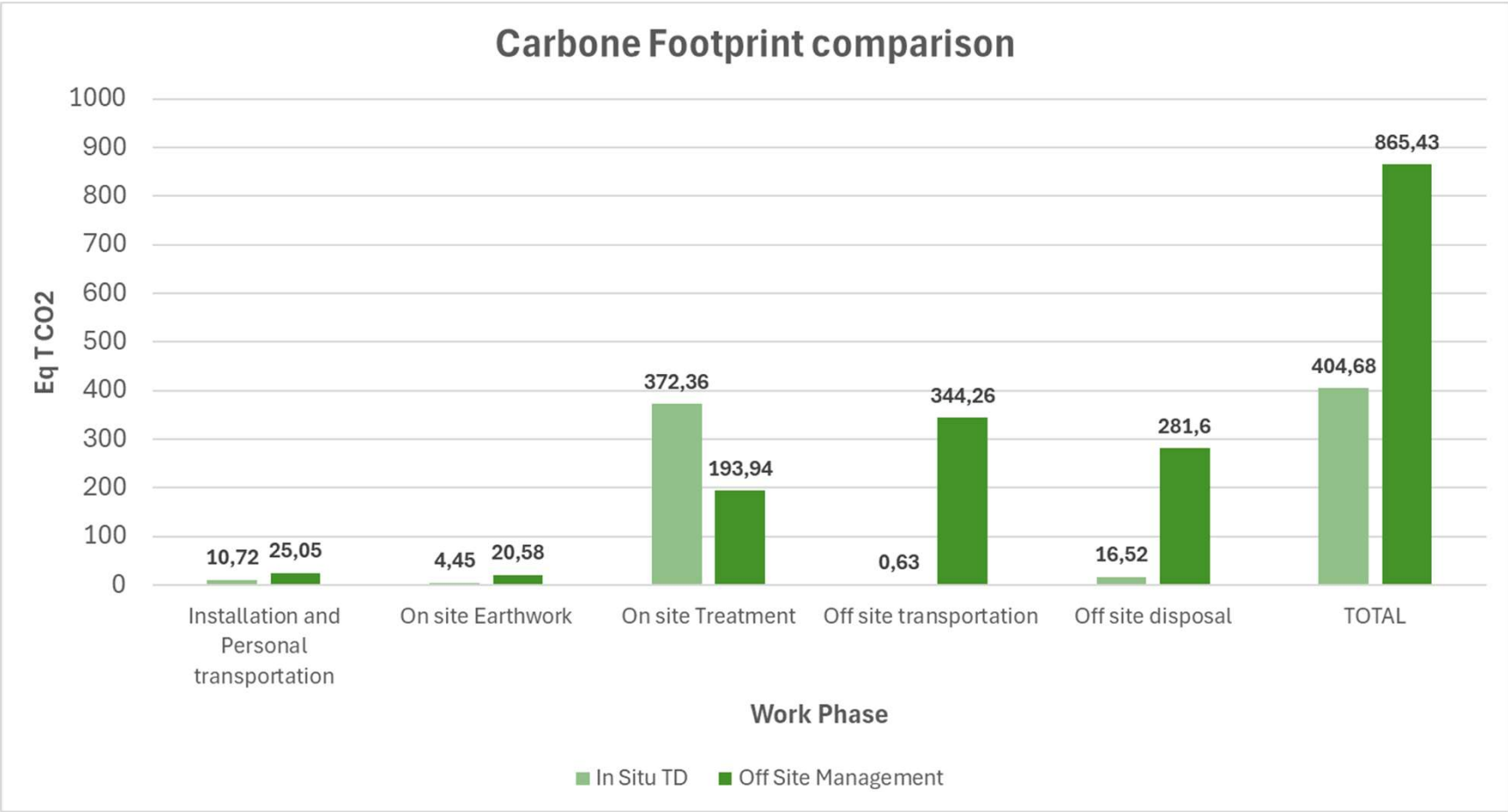
|               | Mercury concentration in the soil after treatment |       |       |       |
|---------------|---|-------|-------|-------|
| [Hg] en mg/kg | ZP1-a   | ZP1-b | ZP1-c | ZP1-d |
| [Hg]min       | 182   | 8     | 8     | 36    |
| [Hg]moy       | 561   | 241   | 96    | 172   |
| [Hg]max       | 784   | 873   | 348   | 722   |

The mass balance of mercury present in the soil was evaluated and adjusted during the works:

- **V1** : 6 boreholes (diag.) – overestimation due to the presence of mercury beads
- **V2** : 10 boreholes (initial state before works) including homogenization of samples
- **V3** : 16 boreholes (V1 + V2), applying the % of mercury that can be mobilized (mercury speciation)
- **V4**: 6 post-work boreholes (final state), applying the % of mercury that can be mobilized.



# Carbon footprint assessment







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